

Efficiency and Design Improvements in Multiple Hearth & Fluid Bed Incinerators

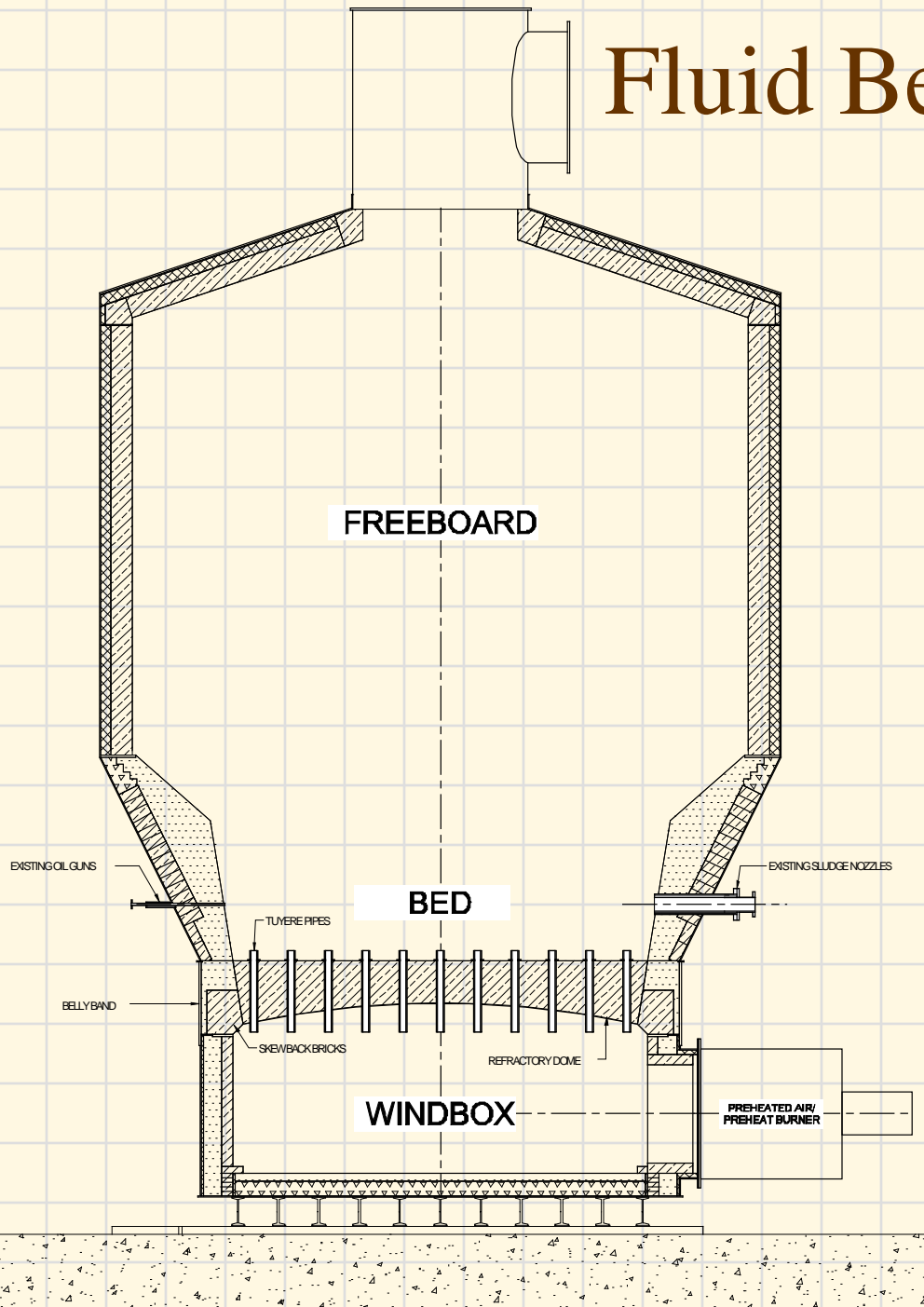
CBE

Chavond-Barry Engineering
400 Rt. 518, Blawenburg, NJ 08504

Outline

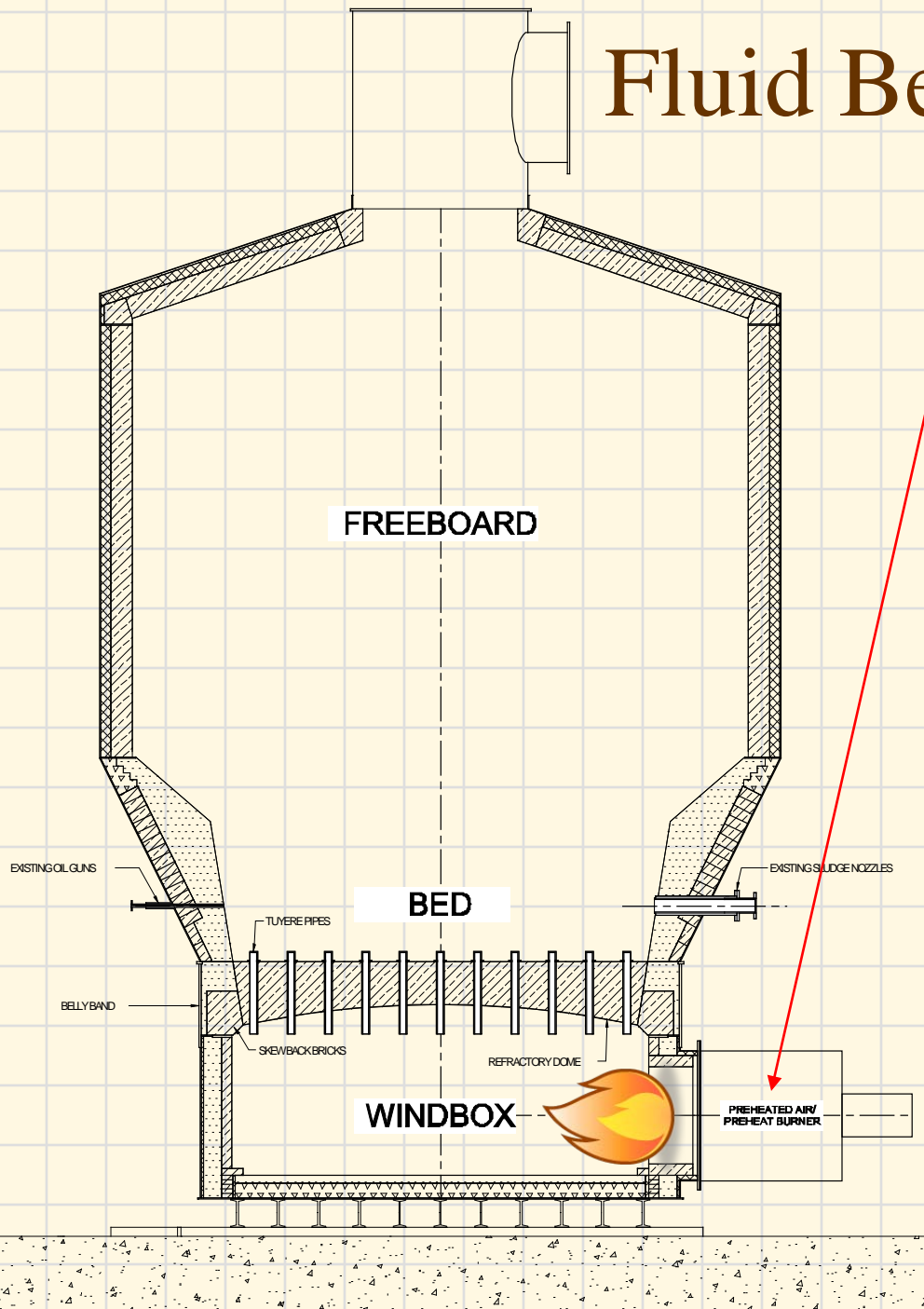
- Fluid Bed Incinerators (FBI's)
 - Reversible Bed Resizing
 - Air Preheating
- Multiple Hearth Incinerators (MHF's)
 - Reheat and Oxidize (RHOX) Process
 - Flue Gas Recirculation (FGR)
 - Center Shaft Air
- General
 - Improved Dewatering
 - Grease

Fluid Bed Incinerator



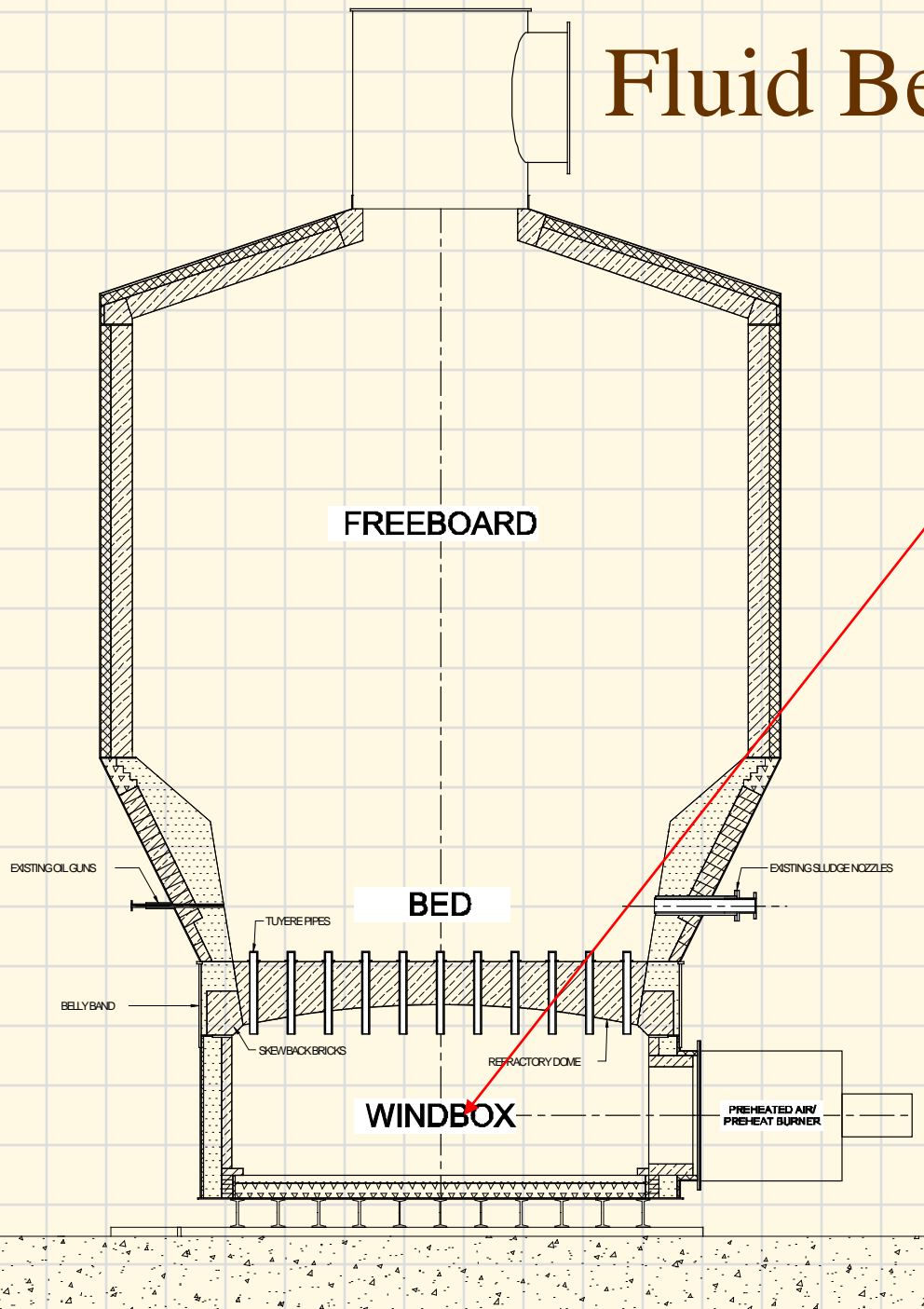
- Preheated Air & Burner
- Windbox
- Dome
- Tuyeres
- Bed
- Freeboard

Fluid Bed Incinerator



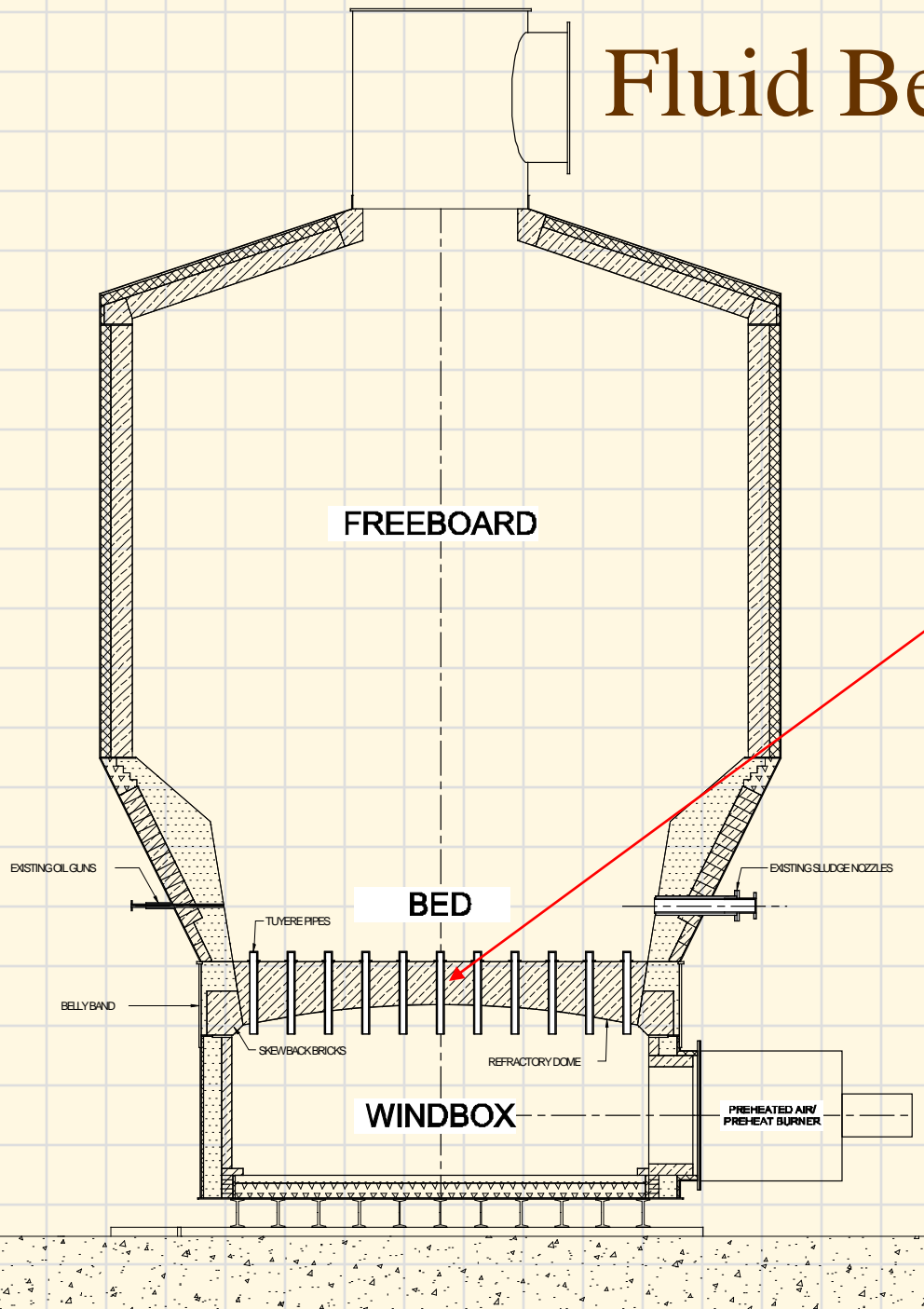
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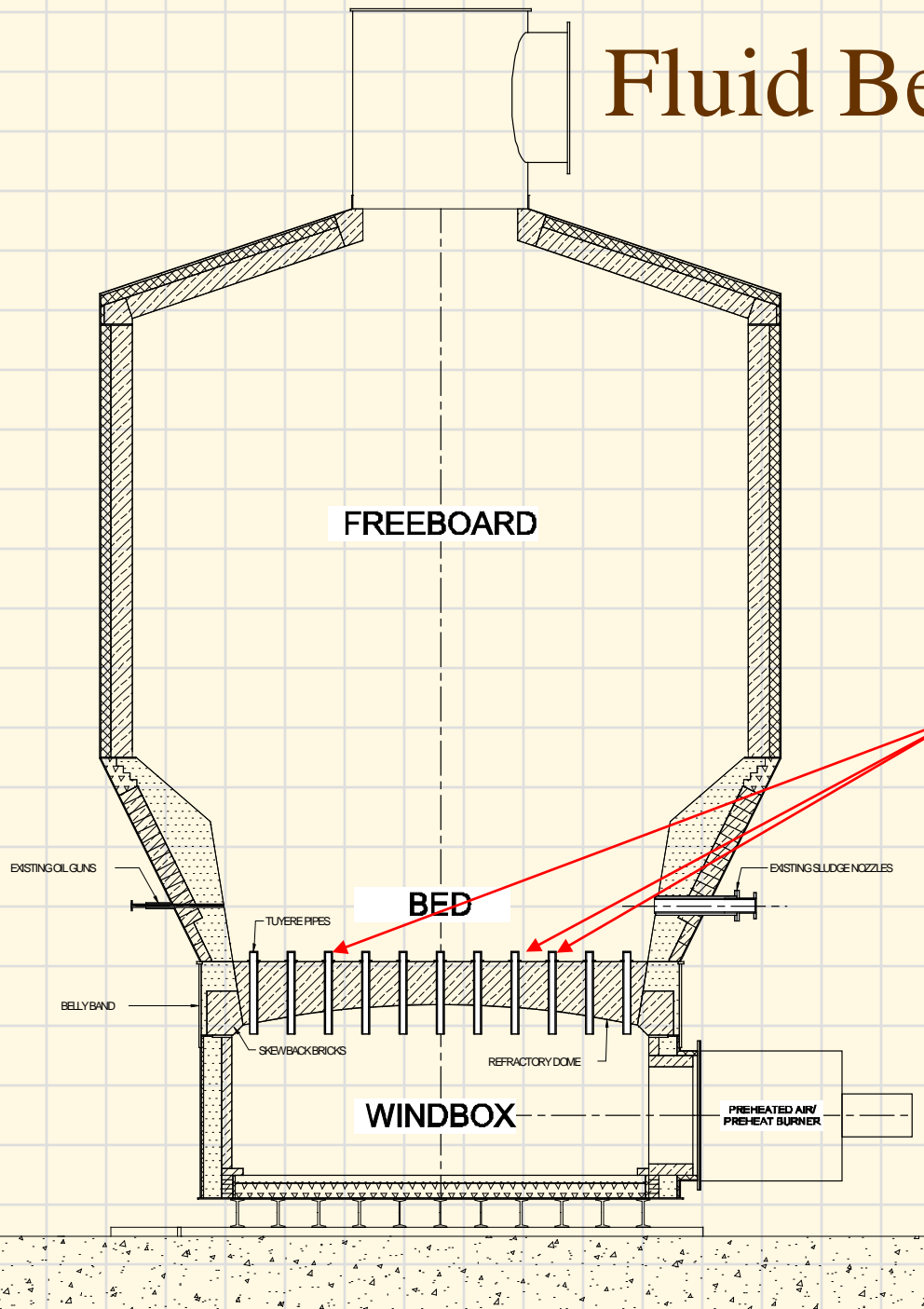
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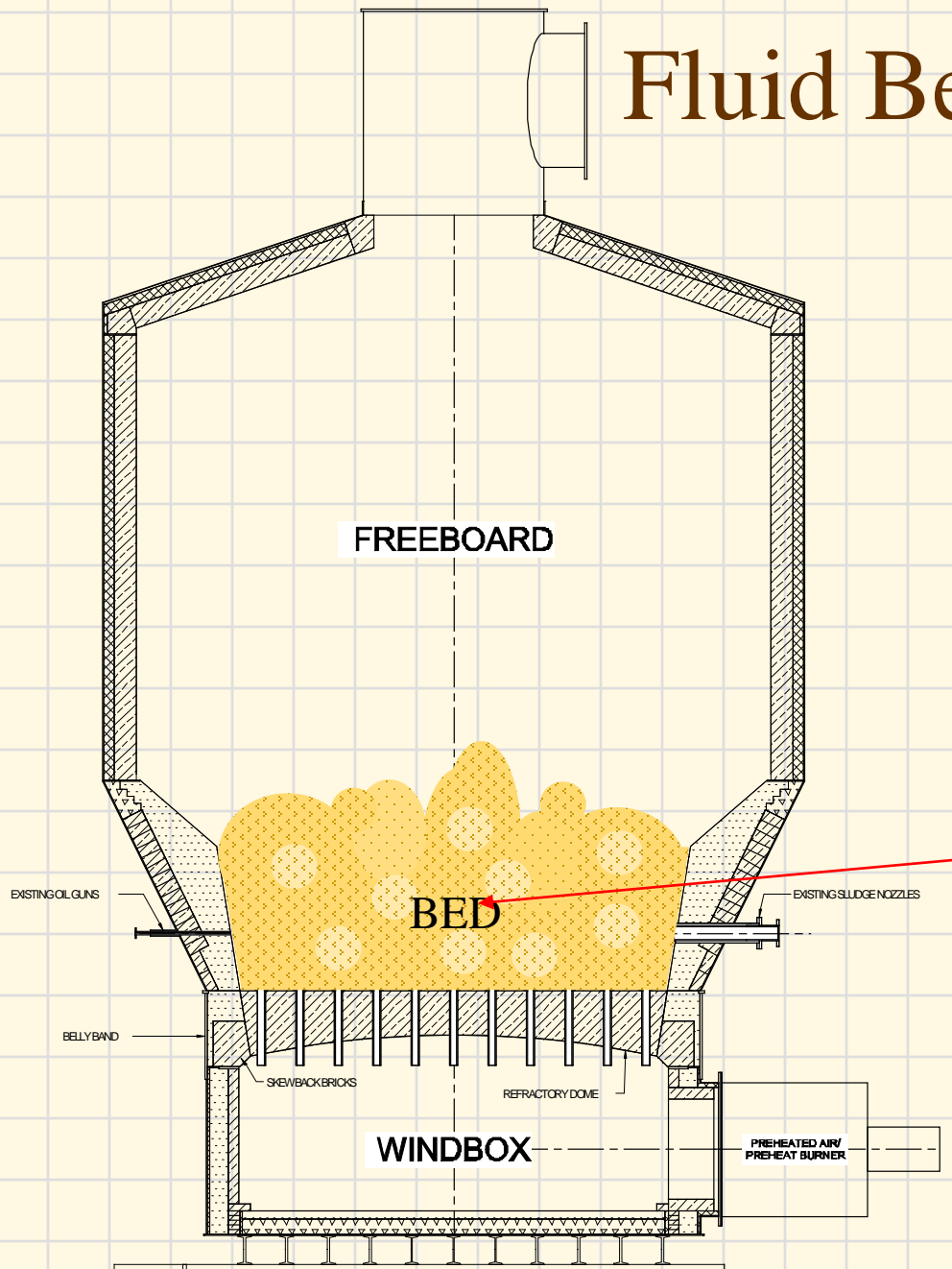
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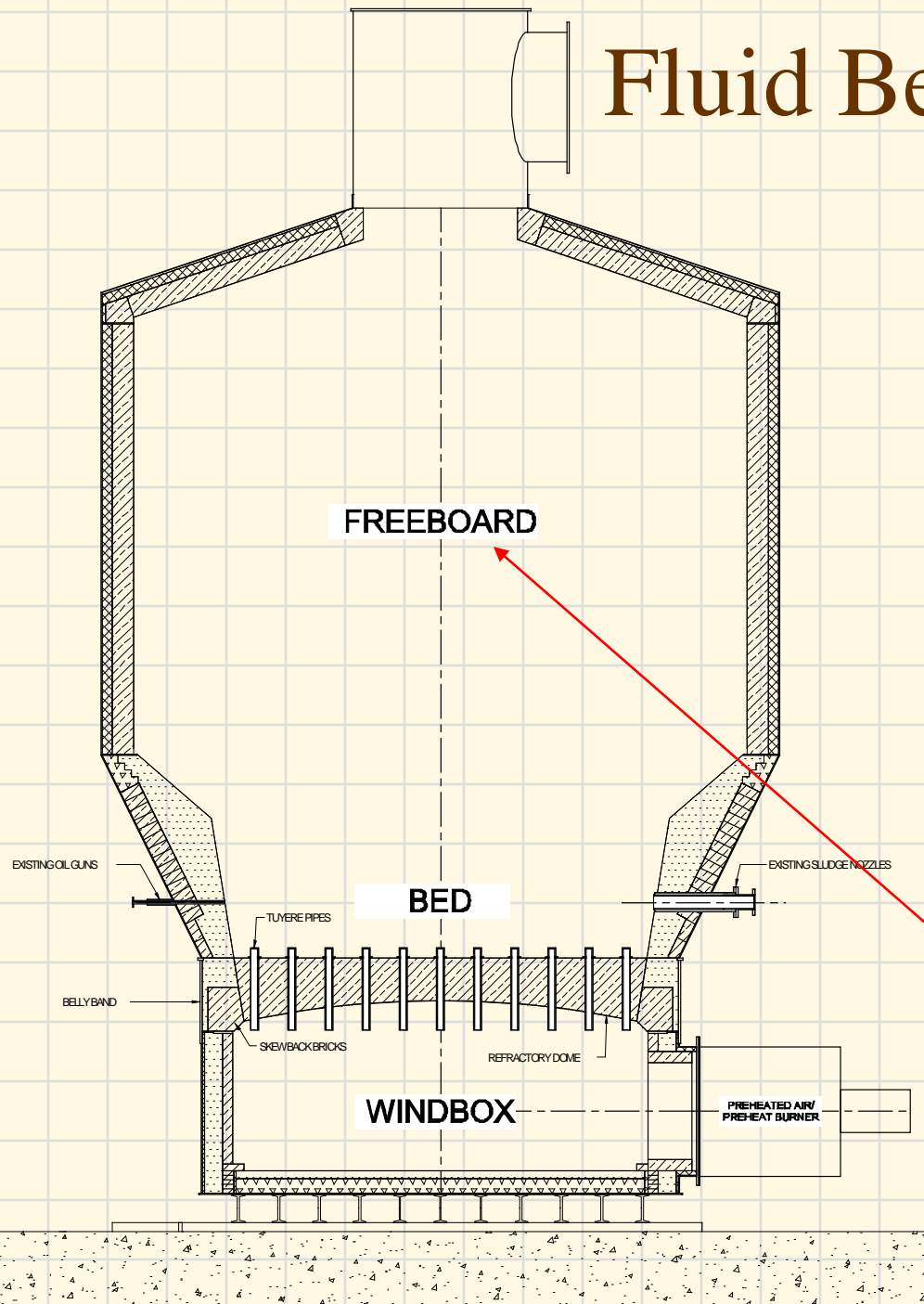
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Fluid Bed Incinerator



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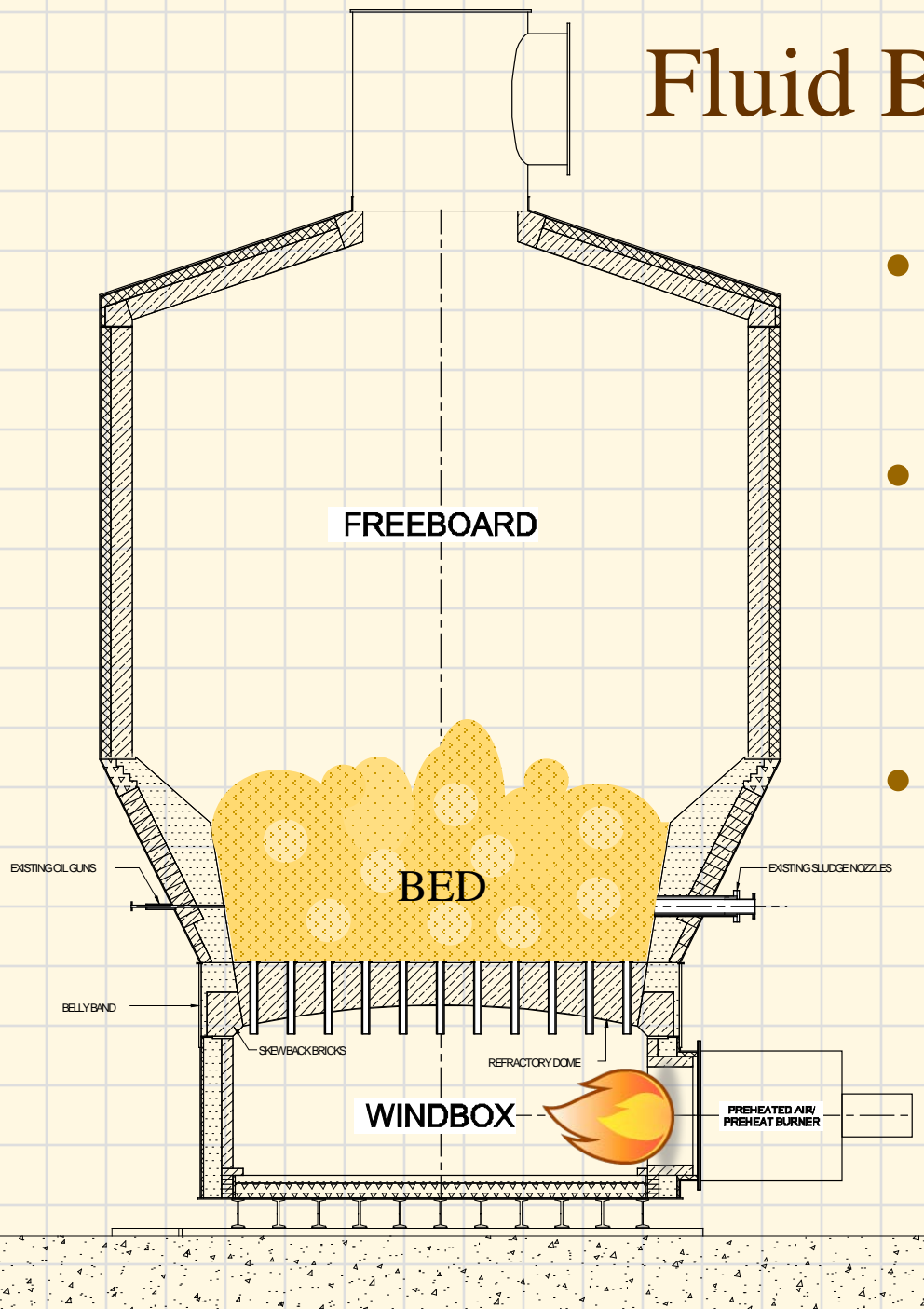
Fluid Bed Incinerator



- Preheated Air & Burner
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- **Freeboard**

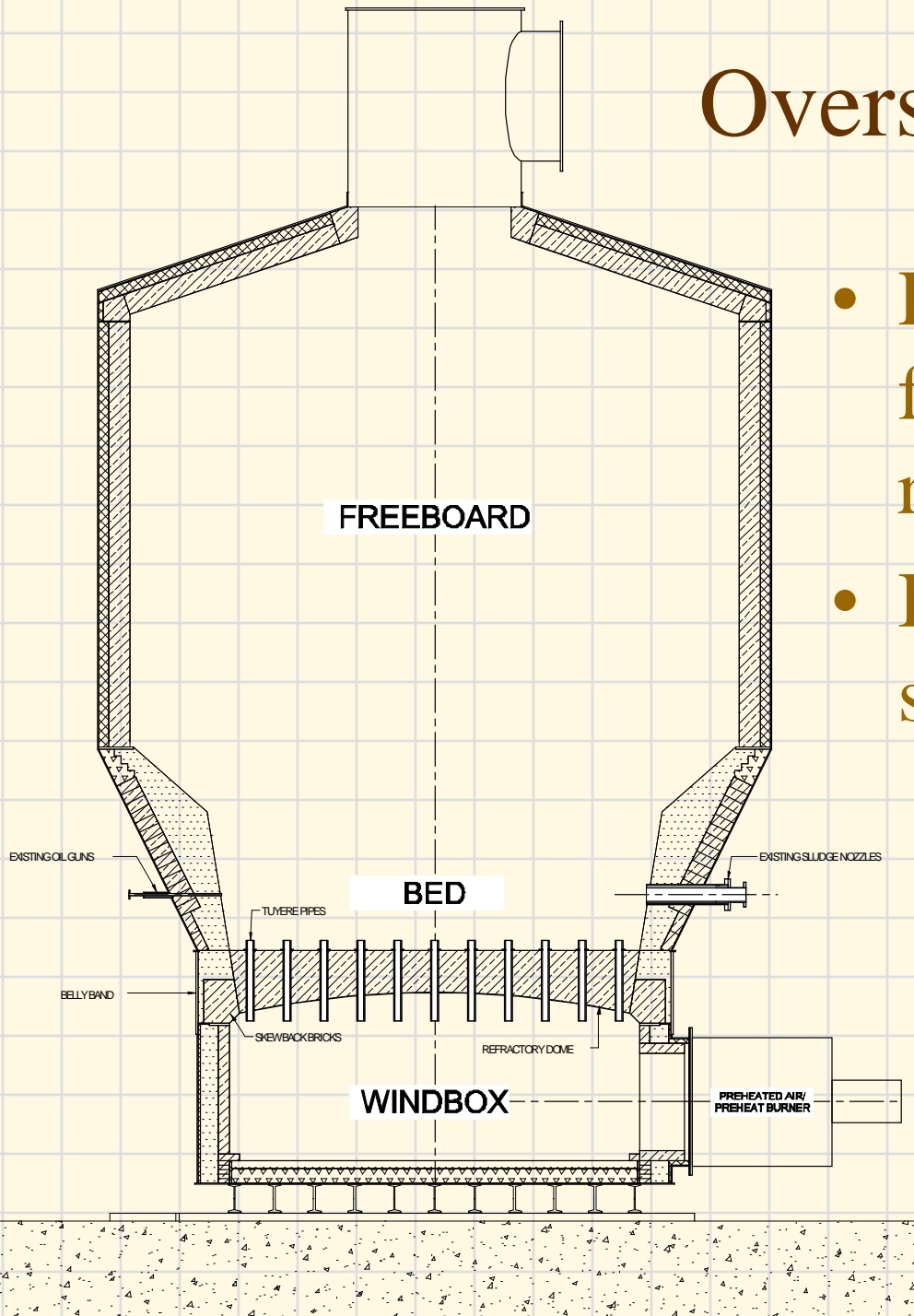
Fluid Bed Incinerator

- Air enters through bottom
- Sludge and fuel introduced in the bed
- Ash and exhaust gasses exit through the top

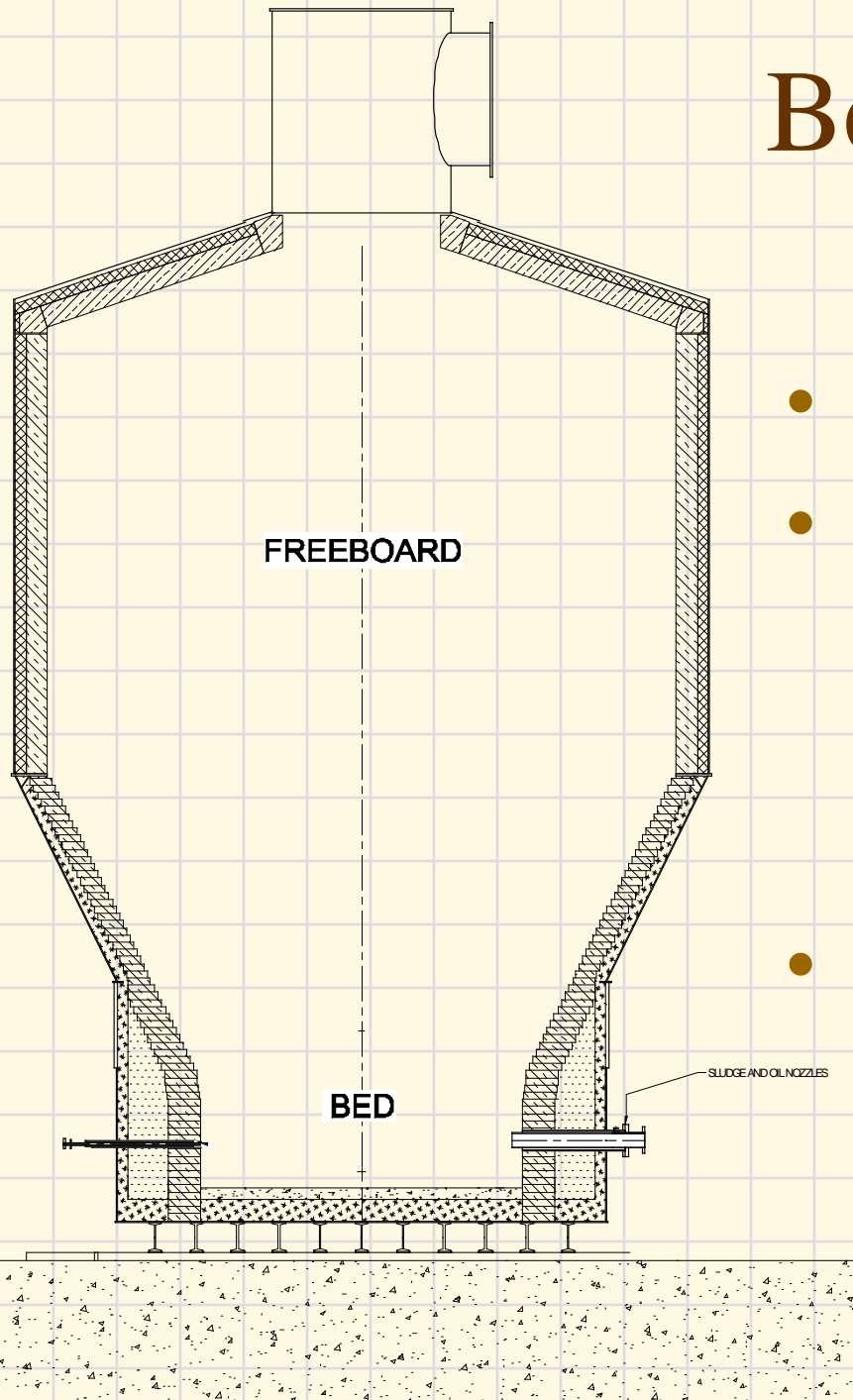


Oversized FBI

- High minimum fluidizing air required
- Inefficient at low sludge feed rates

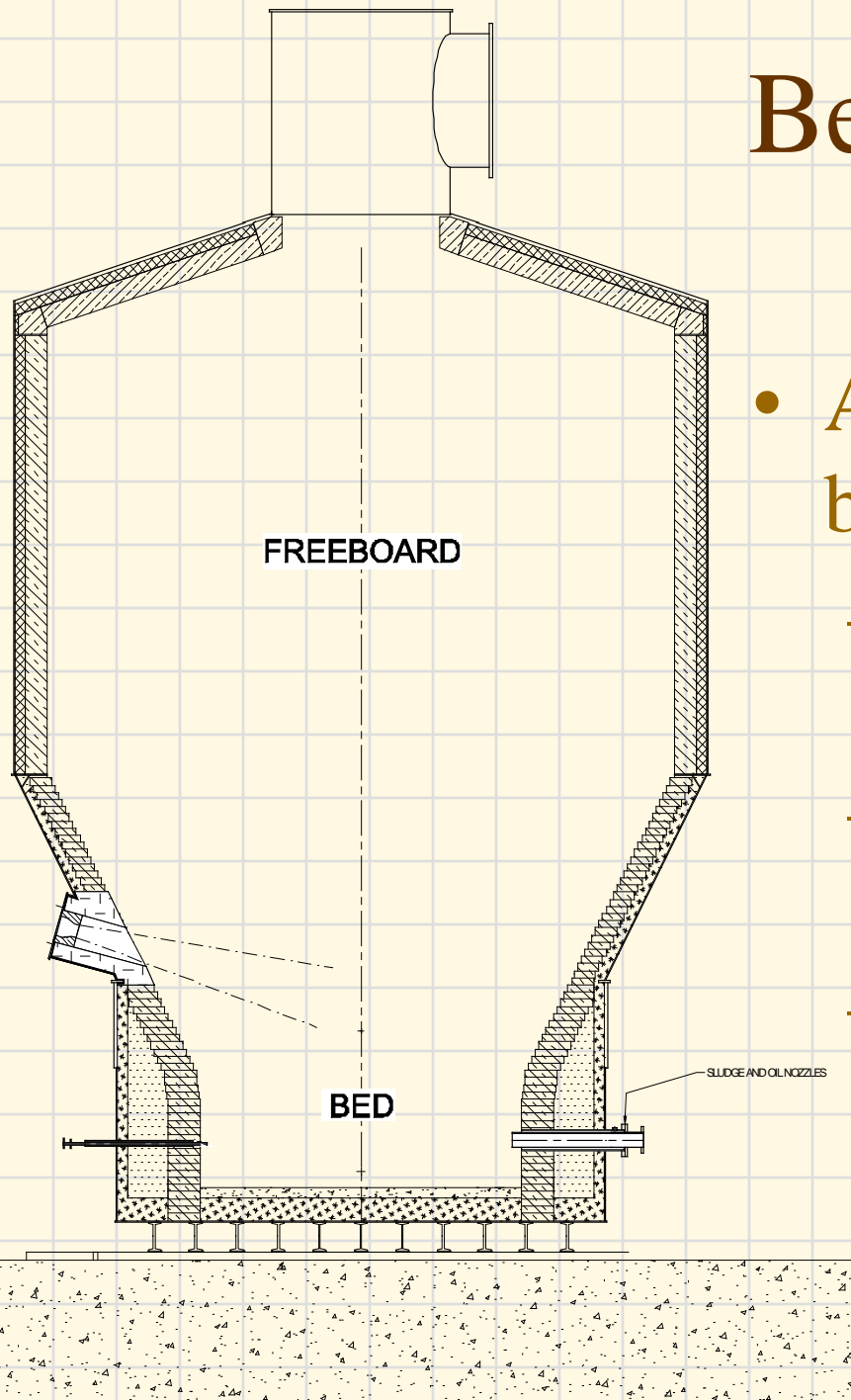


Bed Resizing



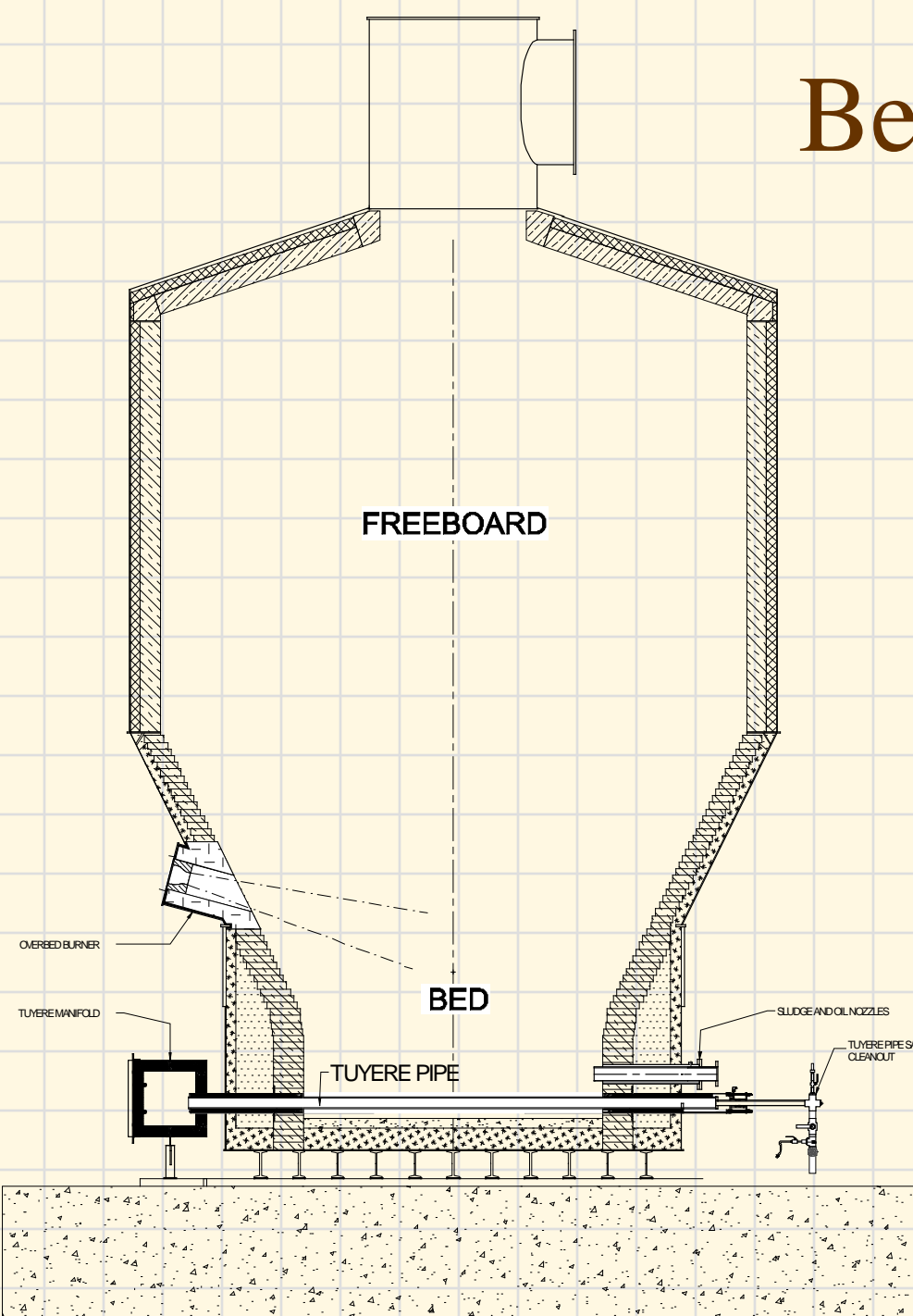
- Remove dome
- Shift bed downward
 - Oil guns
 - Sludge guns
 - Instrumentation
- Shrink diameter of bed

Bed Resizing

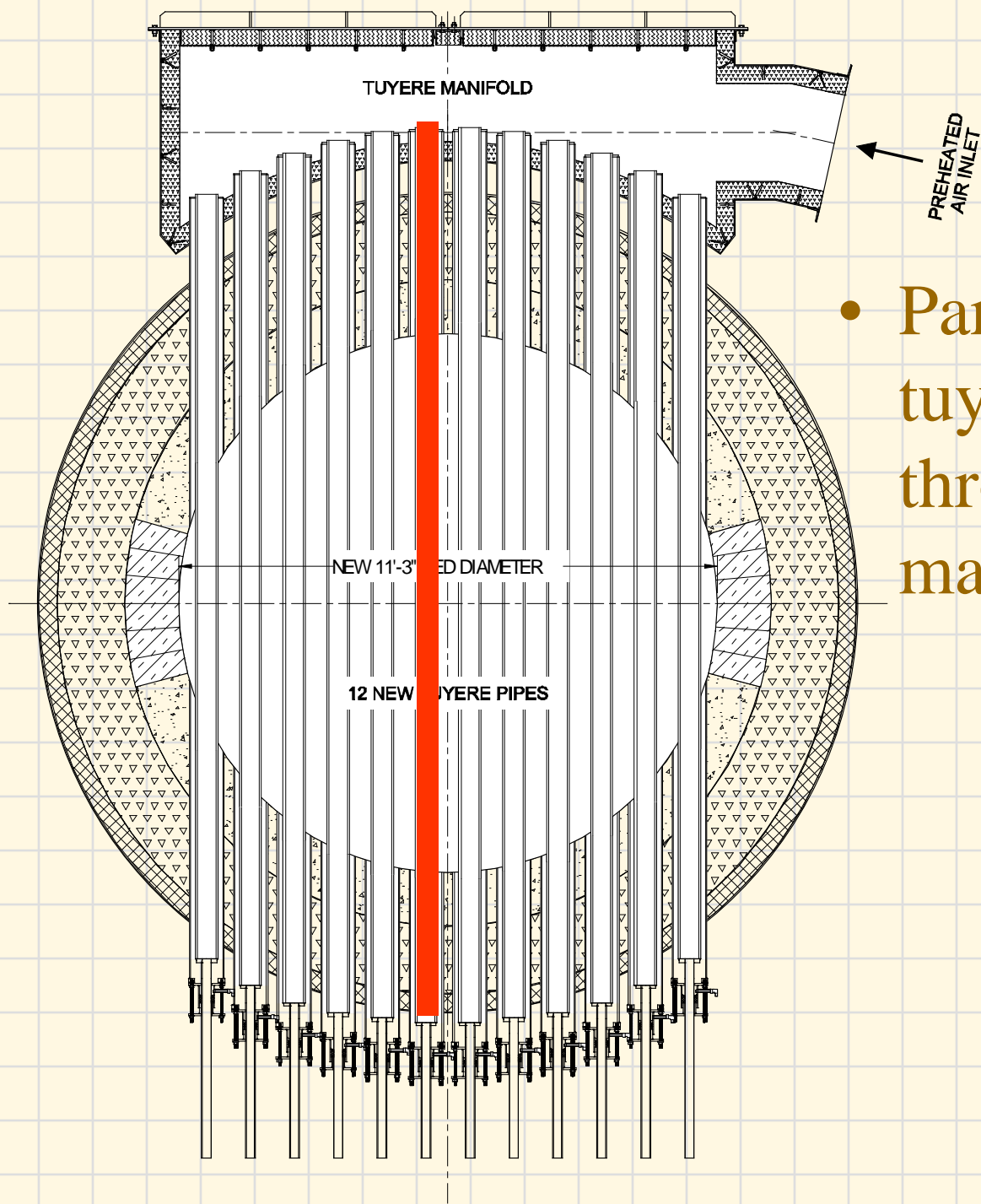


- Add over bed burner
 - Provides live flame in freeboard
 - Directed at top of sand
 - Can be used to heat freeboard directly

Bed Resizing



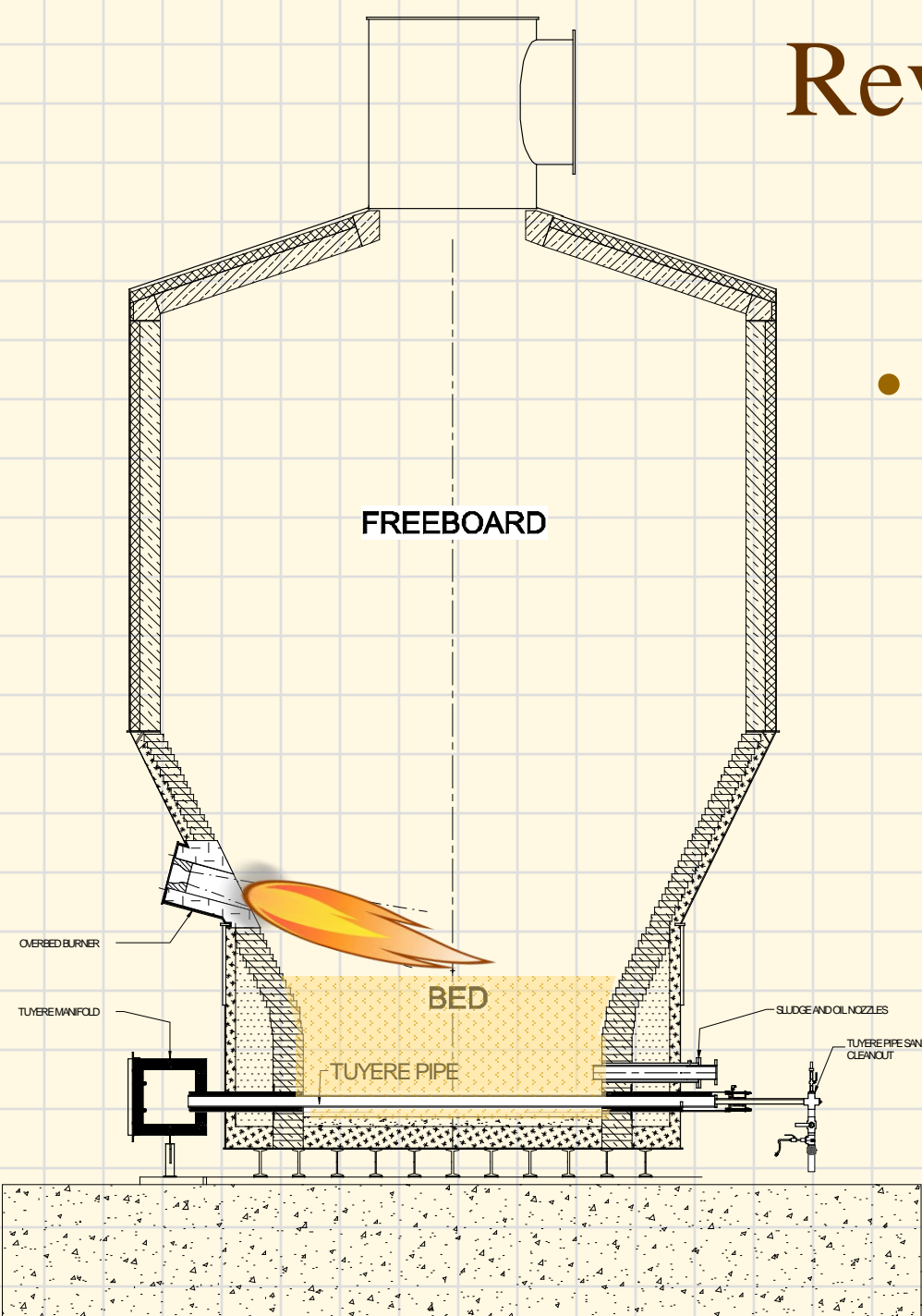
- Pipe Tuyeres
 - Set of parallel pipes
 - Holes in pipes to distribute air
- External air manifold
- Pipe clean out manifold



- Parallel pipe tuyeres receive through external manifold

Reversible Bed Resizing

- Bed can be expanded incrementally back to original size if needed
 - Remove row of bricks
 - Drill additional holes in pipe tuyeres

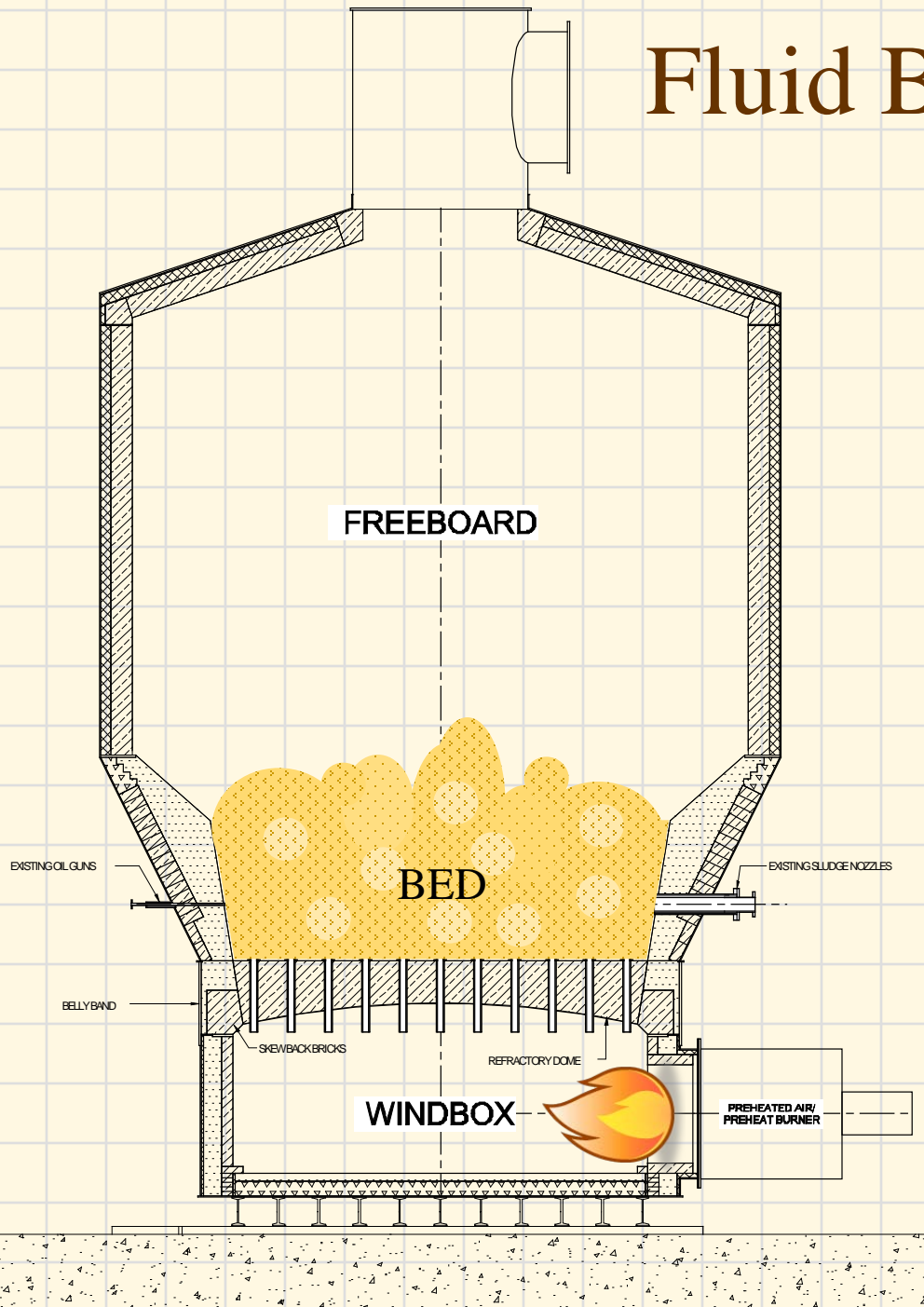


Pipe-Tuyere Design Considerations

- Fluidizing air
 - Blower efficiency at lower air flow
 - Heat exchanger bypass
- Pipe durability
 - No shutdowns from lost tuyeres
 - Can clean-out sand from pipes while operating
 - Can still operate with broken pipe tuyere
- Over-bed burner
 - Improved freeboard temperature control
 - Live flame can reduce CO
 - Better freeboard mixing

Fluid Bed Incinerator

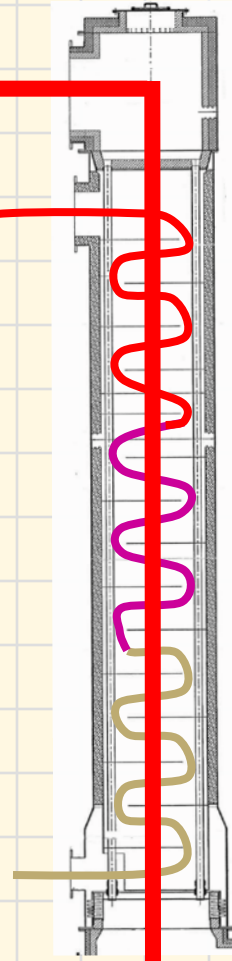
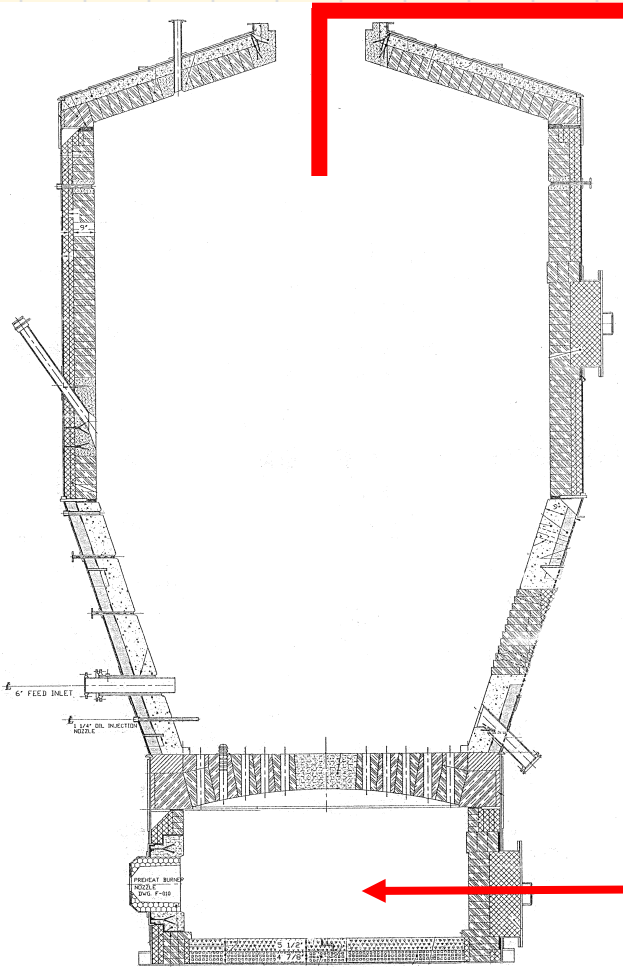
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Preheating the Combustion Air

- Fluidizing air
 - Older FBI designs incorporate no or very low temperature, air preheating
 - Preheating combustion air reduces fuel required during operation
 - Higher preheat temperatures = less auxiliary fuel
 - Often accomplished with a flue gas heat exchanger

FGTT Heat Exchanger



Furnace exhaust flows through the inner tubes of the heat exchanger preheating fluidizing air

Preheating the Combustion Air

- Example:

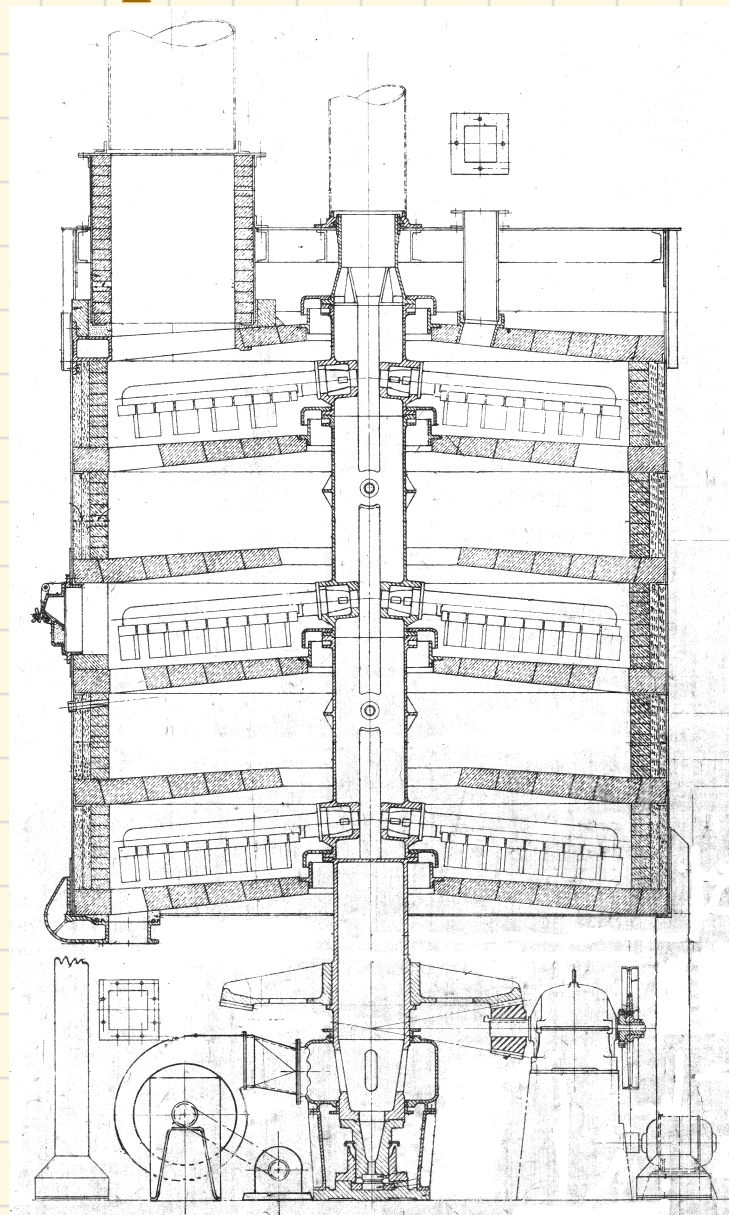
- 5,000 SCFM, Preheated +1000°F

$$.25\text{BTU/lbm}^\circ\text{F} \times .075\text{lbm/ft}^3 \times 5000\text{SCFM} \times 1000^\circ\text{F}$$

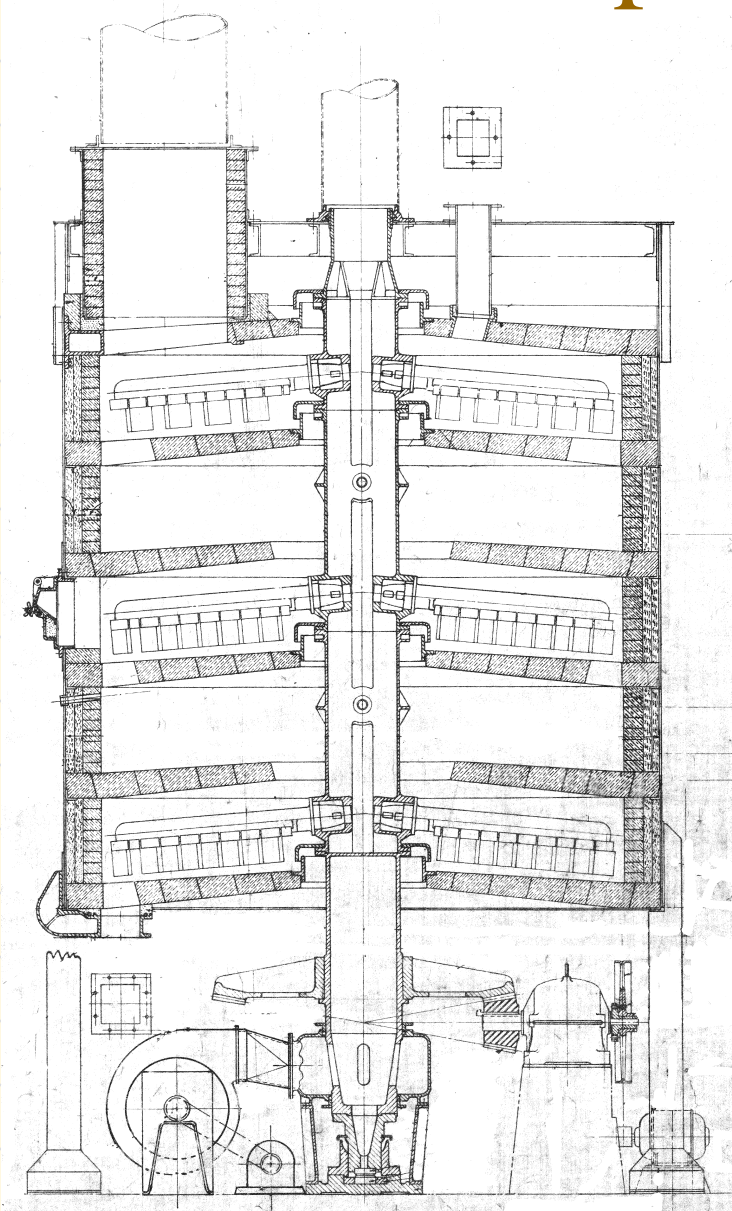
- **93,750 BTU/min, or < 40 gal/hr fuel oil**

$$40\text{ gal/hr} \times 3\$/\text{gal} \times 24\text{hrs/day} = \$2880/\text{day}$$

Multiple Hearth Furnace

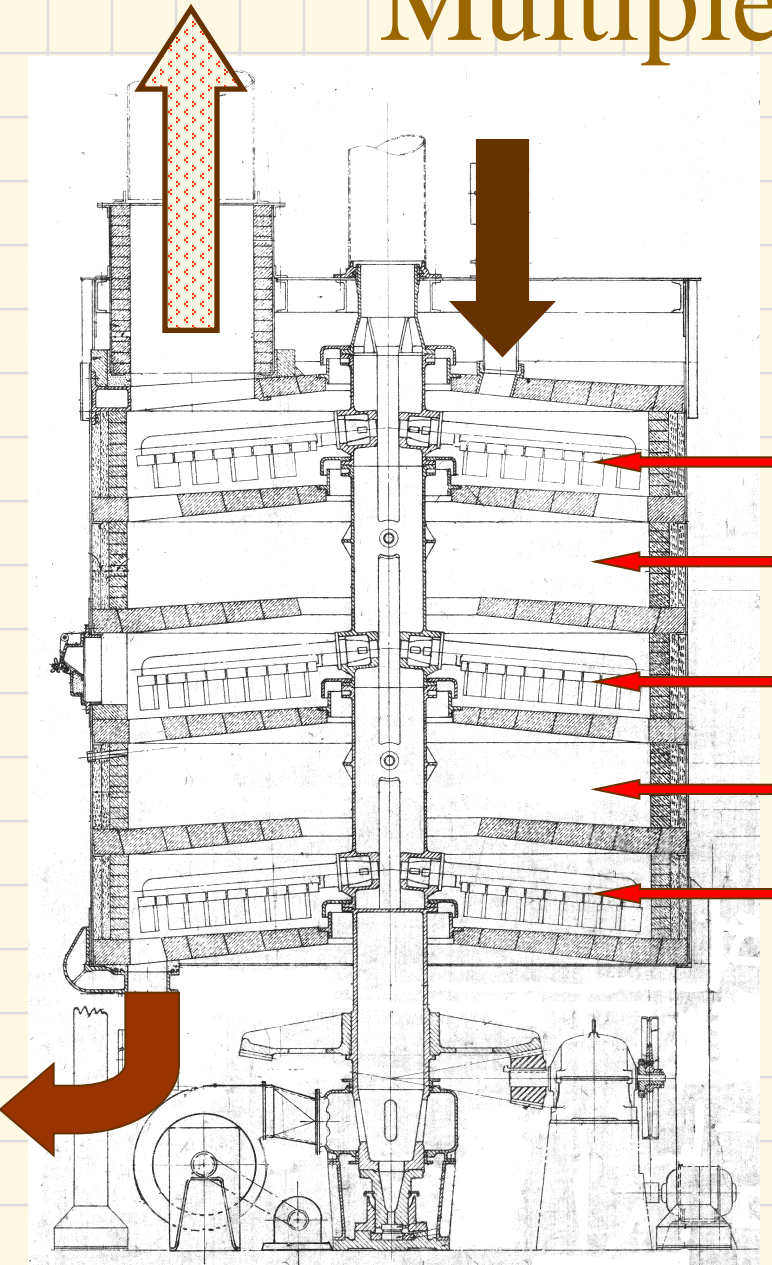


Multiple Hearth Furnace



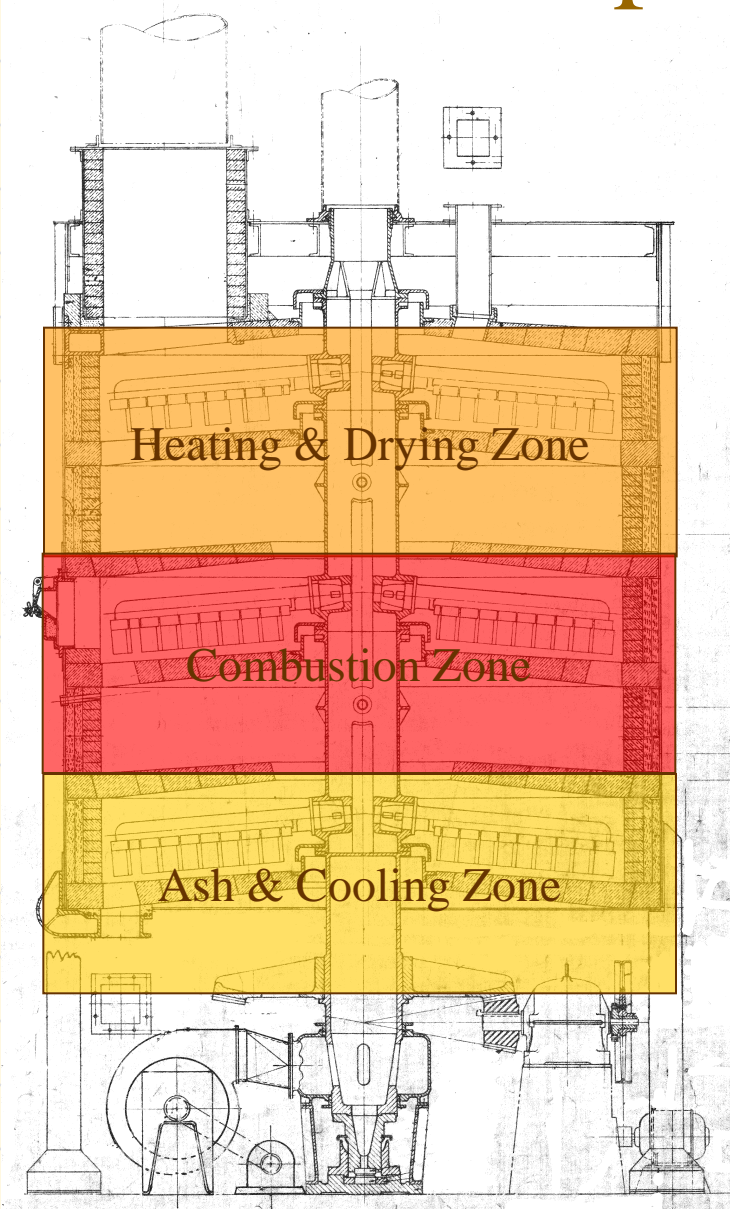
- Refractory lined cylindrical steel shell
- Separated into a series of combustion chambers - refractory hearths one above the other
- Temperature and reaction environment well controlled on each hearth

Multiple Hearth Furnace



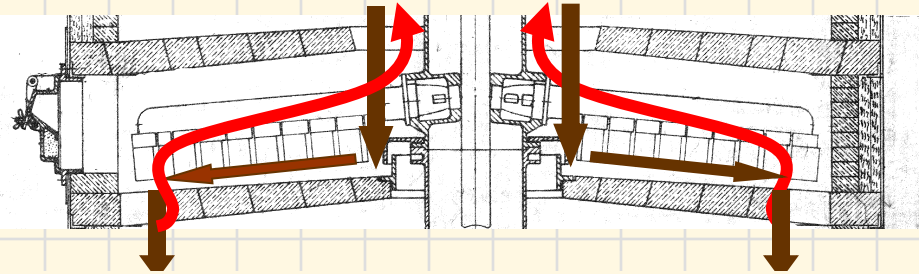
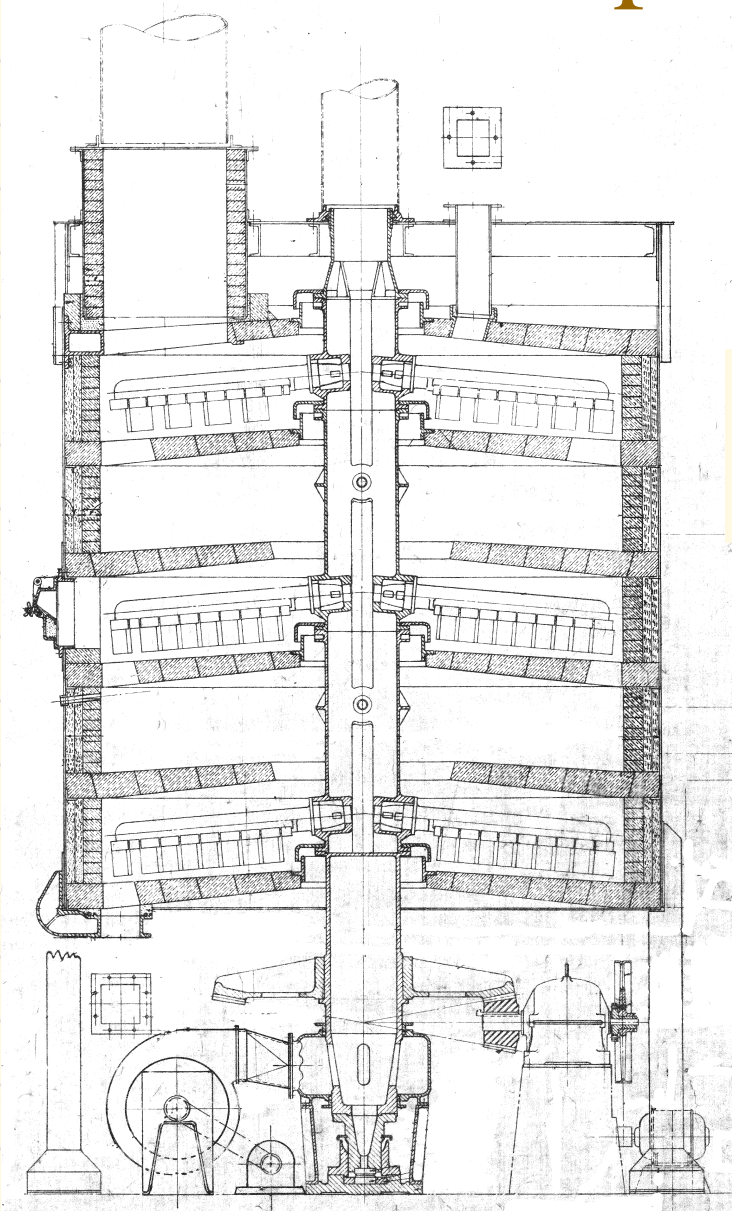
- Dewatered sludge cake enters the furnace at the top
- Inject air and fuel where needed to maintain temperature and supplement the combustion process
- Ash product exits the bottom
- Furnace exhaust gases exit at the top and head to downstream air processing

Multiple Hearth Furnace

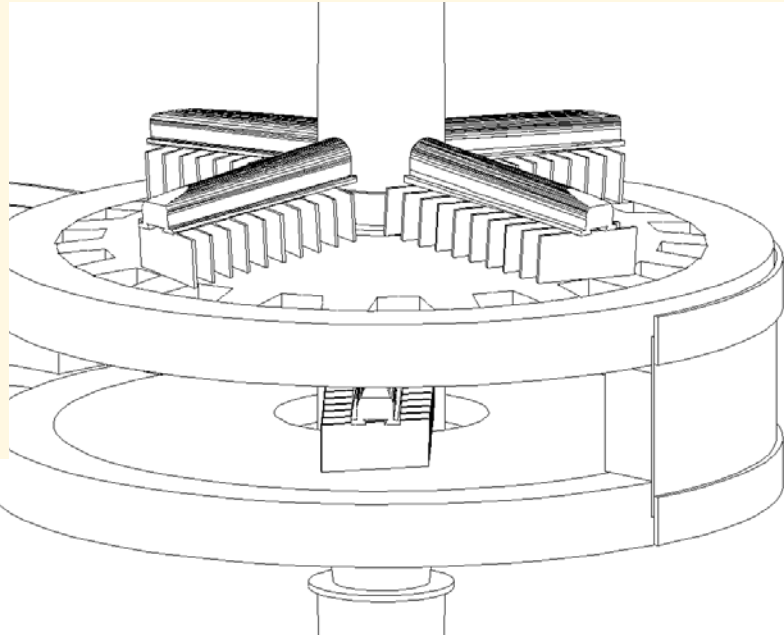


- Dewatered sludge Cake enters the furnace at the top
- Inject air and fuel where needed to maintain temperature and supplement the combustion process
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- **Generalized to three processing “zones”**

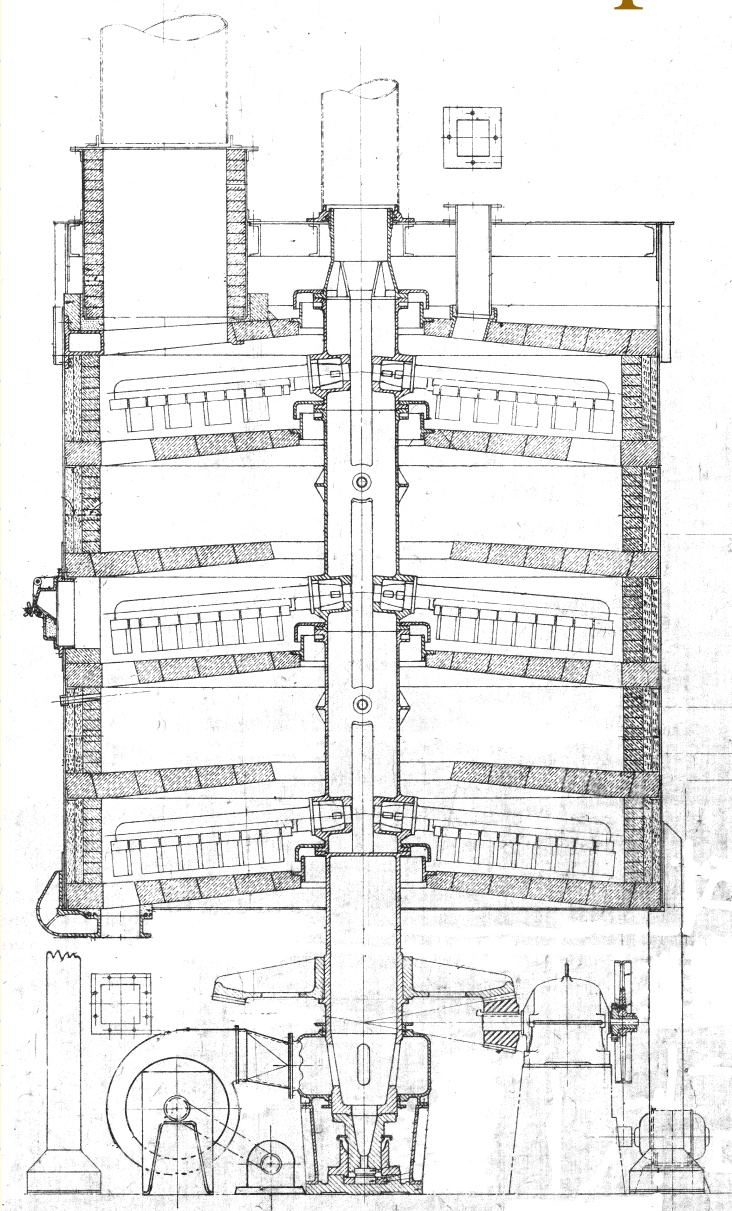
Multiple Hearth Furnace



- Counter current flow of rising exhaust gases and good mixing of descending sludge ensure complete combustion

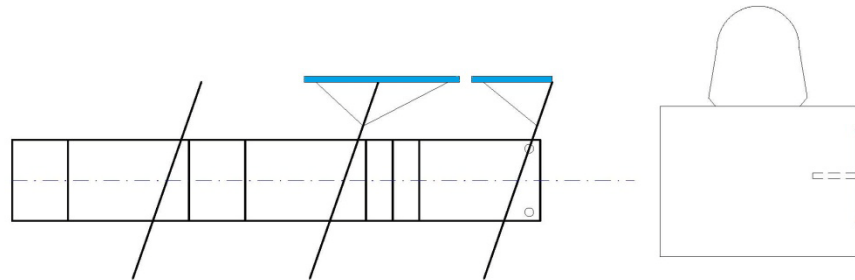


Multiple Hearth Furnace



Poor distribution of sludge across top hearth:

- Under utilization of furnace area, less efficient operation
- Uneven hearth temperatures
- Burning in lower hearths



Adding rabble improves sludge distribution

RHOX – Reheat & Oxidize Process

- In NJ, all MHF are required to maintain an afterburner at $>1500^{\circ}\text{F}$
- Typical afterburner designs include:
 - Top Hearth
 - Top heath with Jumper Flue
 - External Chamber
- Afterburners located directly after the incinerator (before APC equipment)

RHOX – Reheat & Oxidize Process

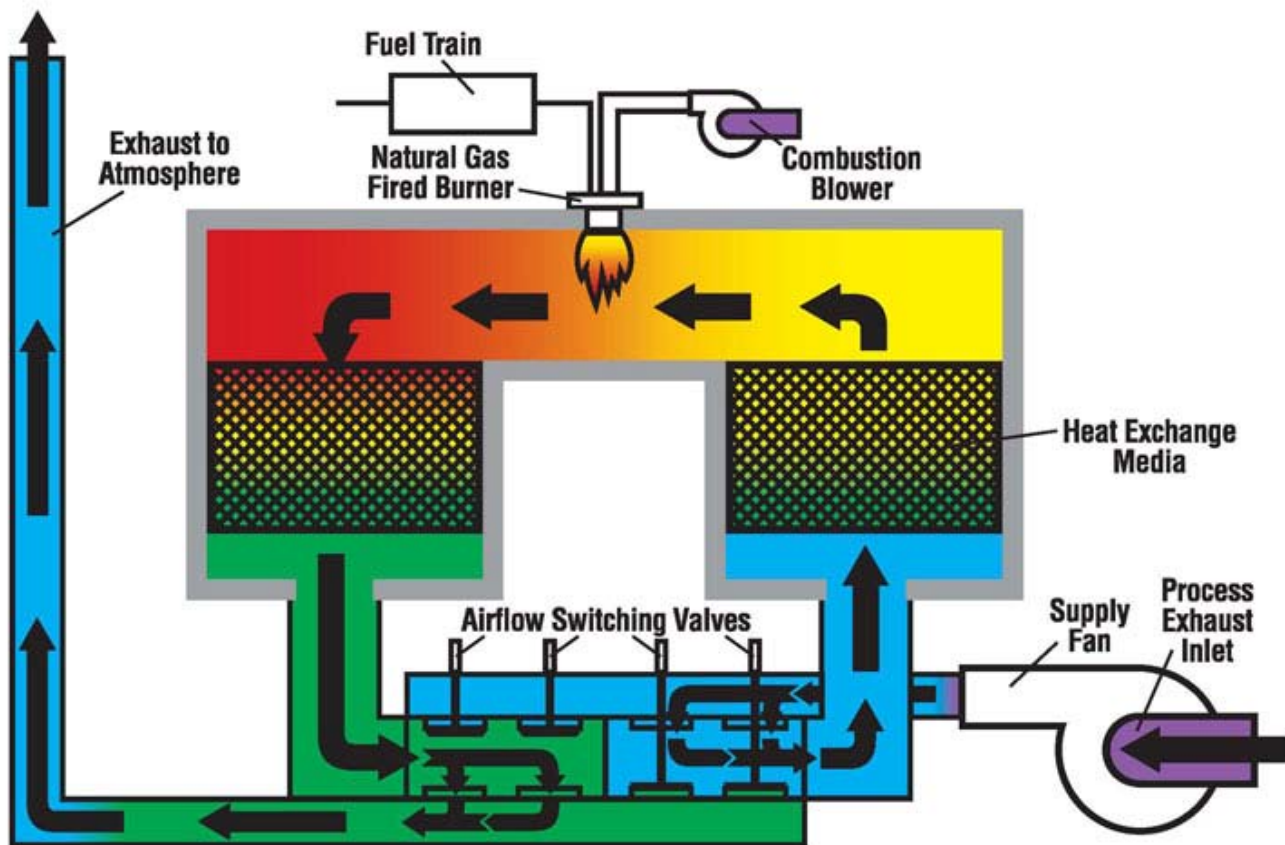
- Traditional afterburner designs require 1 or more burners
- Require high fuel usage to maintain afterburner temperature
- Additional burners can produce NO_x

RHOX – Reheat & Oxidize Process

- RHOX Process differs in that:
 - Occurs after the APC equipment
 - Recovers heat from exiting exhaust gasses
 - Requires 1 burner (less potential Nox production)
- Common RHOX process application is the Regenerative Thermal Oxidizer (RTO)

Regenerative thermal Oxidizer

Regenerative Thermal Oxidizer
Airflow Diagram



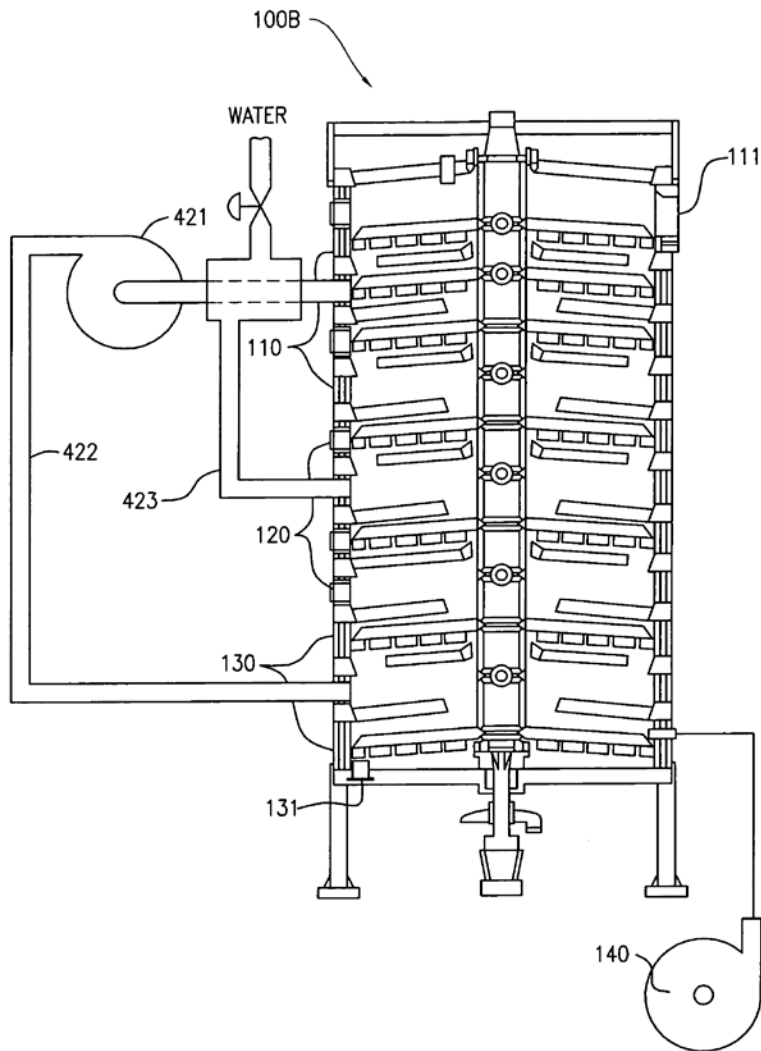
Regenerative Thermal Oxidizer

- RTO:
 - Utilizes 2 or more heat recovery chambers
 - Cold inlet gas passes through a heated chamber, preheating the gas
 - Hot exhaust exits through and heats another chamber
 - A single burner maintains gas temperature within the RTO
 - Periodically, a valve switches the inlet/outlet chambers

Regenerative Thermal Oxidizer

- RTO benefits:
 - More efficient than traditional afterburners
 - The use of waste heat recovery decreases the fuel requirements
 - Provides more control than traditional afterburners
 - Less affected by furnace upsets / changes

Flue Gas Recirculation (FGR)



- Another efficiency improvement for MHF's is Flue Gas Recirculation
- FGR moves exhaust gas from the feed (top) hearth to a hearth below the volatile burning zone

Flue Gas Recirculation (FGR)

- FGR
 - Injection of cooler mostly inert gas:
 - Reduces fuel usage
 - Increases operational stability
 - Reduces slag formation
 - Lowers hearth peak temps
 - Reduces oxygen content
 - Increases operational stability
 - Reduces flare-up during feed stoppage
 - Promotes complete ash burnout
 - Better solids gas phase mixing
- lowering NO_x production

Flue Gas Recirculation (FGR)

- Hearth without FGR (Left) and with (Right)



Center Shaft Air

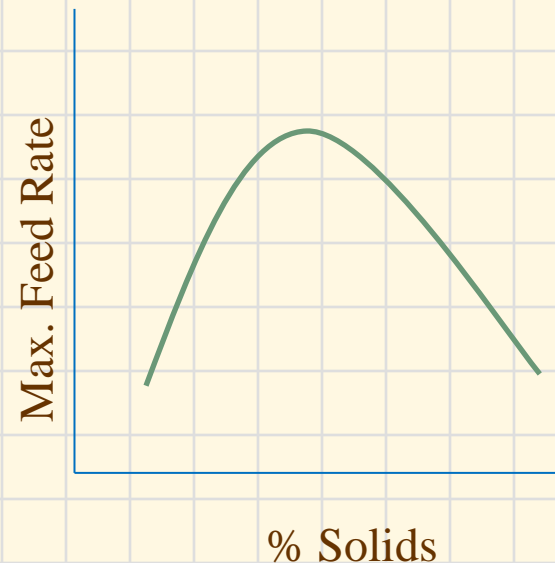
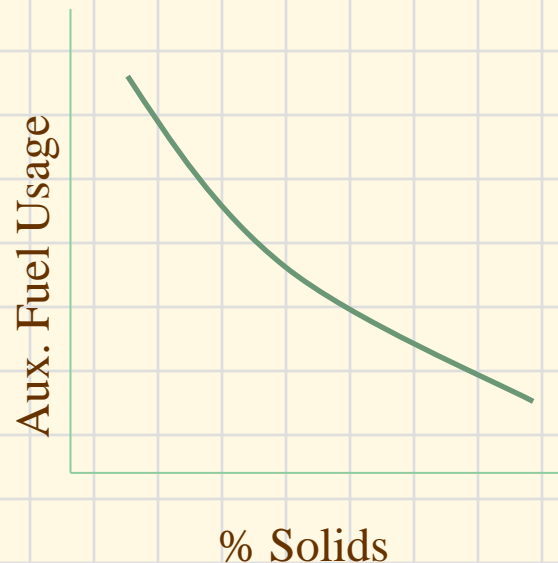
- Another way to reduce fuel usage in MHF's is by utilizing heated Center Shaft Air
- The Center shafts and rabble arms are air cooled
- Heated center shaft air can be:
 - Injected into the stack for steam plume suppression & increased dispersion
 - Utilized as burner air supply or furnace combustion air to decrease fuel usage

Improved Dewatering

- Typical Sludge Cake
 - Belt filter press: <21-25% solids
 - Centrifuge: 27-30% solids
 - ~75% water
- Why does this matter?
 - Heating Value of Water = 0
 - Water requires a large heat *input* to vaporize
$$\Delta H_{vap} = -1059 \text{ BTU/lb}$$
- More water = More auxiliary fuel

Improved Dewatering

- At low moisture content, sludge can burn without the addition of fuel oil (Autogenous).
- Typically at $>26\%$ for a Fluid Bed
- Super-Autogenous conditions limit operations



Fat, Oil & Grease

- Fat, Oil, and Grease are waste-products from the restaurant industry
- Consists of some food debris, mostly cooking oils & fats, and ~96% water
- Often concentrated to <50% water before added to an incinerator
- Grease can be used to supplement auxiliary fuel (sometimes up to 100% during operation)

Fat, Oil & Grease

- No petroleum products or other hazardous materials found in grease
- Non-processed fuel (concentrating aside)
- Restaurants typically pay a tipping fee for removal and disposal
- With current fuel prices, R.O.I. for a grease receiving/handling facility can be less than 3 years with tipping fees or 6 years without



Questions?

Chavond-Barry Engineering Corp.

400 County Route 518

Blawenburg, NJ 08504

Tel: (609) 466-4900

Fax: (609) 466-1231

CBE